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CHEMICAL ENGINEERING



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Corporate Office: 44-A/4, Kalu Sarai, New Delhi-110016

Ph. : 9021300500 | **E-mail:** infomep@madeeasy.in

2200+ Solved Questions

for

GATE, PSUs & State Engineering Examinations

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P r e f a c e

This Chemical Engineering practice book containing nearly 2200+ solved questions focuses in-depth understanding of subjects which has been segregated topicwise to disseminate all kind of exposure to students in terms of quick learning and deep apt. The topicwise segregation has been done to align with contemporary competitive examination pattern. Attempt has been made to bring out all kind of probable competitive questions for the aspirants preparing for GATE, PSUs and State Engg. Exams. The content of this book ensures threshold level of learning and wide range of practice questions which is very much essential to boost the exam time confidence level and ultimately to succeed in all prestigious engineers' examinations. It has been ensured from MADE EASY team to have broad coverage of subjects at chapter level.

While preparing this book utmost care has been taken to cover all the chapters and variety of concepts which may be asked in the exams. The solutions and answers provided are upto the closest possible accuracy. The full efforts have been made by MADE EASY Team to provide error free solutions and explanations.

I have true desire to serve student community by way of providing good sources of study and quality guidance. I hope, this book will be proved an important tool to succeed in competitive examinations. Any suggestions from the readers for the improvement of this book are most welcome.



B. Singh (Ex. IES)

B. Singh (Ex. IES)

CMD, MADE EASY Group

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UNIT 1

Process Calculations

1. Composition and Degree of Freedom

- (b) It relates the number of extensive independent thermodynamics properties for each phase and the number of phases for a system.
 - (c) It relates the number of intensive independent thermodynamic properties for each phase and the number of phases for a system.
 - (d) For a system that does not experience a chemical reaction, the Gibbs phase rule reads as follows:
 $\pi + f = N + 2$, where
 π = Phases
 N = Components
 f = Number of intensive independent properties

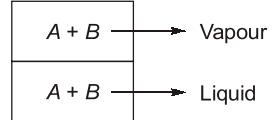
f = Number of intensive independent properties

- Q.6** The degree of freedom for the case of pure liquid water and solid ice in equilibrium is _____.

Q.7 The degree of freedom for the case of pure liquid water, solid ice and water vapour in equilibrium is _____.

Q.8 The degree of freedom for the case of solid ice in equilibrium with a liquid mixture of ethanol + water is _____.

Q.9 Consider the following diagram for the mixture of A and B which are in equilibrium, the required degree of freedom is _____.



- Q.10** Which of the following statement is correct about the degree of freedom?

 - (a) Degree of freedom is equal to the number of independent variables present in the system minus the number of equations of constraint between the variables.
 - (b) Degree of freedom is equal to the number of dependent variables present in the system minus the number of equations of constraint between the variables

- (c) Degree of freedom is equal to the number of independent variables present in the system plus the number of equations of constraint between the variables.
 - (d) Degree of freedom is equal to the number of dependent variables present in the system minus the number of equations of constraint between the variables.

2. Basic Chemical Calculations

Q.12 Real gases approach ideal behaviour at
(a) high pressure and high temperature
(b) low pressure and high temperature
(c) high pressure and low temperature
(d) low pressure and low temperature

Q.13 In general, the specific heat of aqueous solution _____ with increase in the concentration of the solute.

- (a) Increase
- (b) Decrease
- (c) Remains unchanged
- (d) Increase then decrease

Q.14 Isotonic solutions must have the same

- (a) Viscosity
- (b) molar concentrations
- (c) Normality
- (d) Critical temperature

Q.15 If M_A and M_B are the molecular weight of component A and B respectively, then the mole fraction (X_A) and weight fraction (X'_A) of component A in a binary mixture of A and B are related by

(a) $X'_A = X_A$

$$(b) \quad X_A' = \frac{\left(\frac{M_B}{M_A}\right)X_A}{1 + \left[\left(\frac{M_B}{M_A}\right) - 1\right]X_A}$$

$$(c) \quad X_A' = \frac{M_A}{M_B} \cdot \frac{X_A}{(1 + X_A)}$$

$$(d) \quad X_A' = \frac{\left(\frac{M_A}{M_B}\right)X_A}{1 + \left[\left(\frac{M_A}{M_B} - 1\right)\right]X_A}$$

Q.16 Fixed carbon content reported in the proximate analysis of solid fuels is always _____, the carbon content reported in the ultimate analysis of solid fuels.

- (a) Equal to
- (b) Lower than
- (c) Higher than
- (d) Higher than or equal to

Q.17 The concentration of SO_2 in the flue gases from a boiler was found to be 0.4 kg/m^3 at N.T.P., the concentration of SO_2 in parts per million by volume at NTP is $m \times 10^4$. Assume that the gases are perfect. The value of m is _____.

Q.18 20 kg of A is fed to a batch reactor where reaction takes place to form a product B. If M_A and M_B are the molecular weight of A and B respectively, then which of the following conclusion is correct?

- (a) Total number of moles decreases as reaction proceed, if $M_A > M_B$.
- (b) Total number of moles increases, if $M_A < M_B$.
- (c) Total number of moles decreases as reaction proceed, if $M_A < M_B$.
- (d) Total number of moles are constant and does not depend on the M_A and M_B .

Q.19 A solution is made by dissolving 1 kilo mole of solute in 2000 kg of solvent. The molality of the solution is _____. [Rounded off to 1 decimal place]

Q.20 The weight fraction of methanol in an aqueous solution is 0.64. The mole fraction of methanol (X_m) is _____. [Rounded off to 1 decimal place]

- Q.38** The value of overall conversion is (in %) _____. [Rounded off to 2 decimal places]
- Q.39** Air to ethylene mole ratio in the feed mixture is
 (a) 1 : 16.81 (b) 16.81 : 1
 (c) 1 : 24.2 (d) 24.2 : 1
- Q.40** 20000 kg of a 5% slurry of calcium hydroxide in water is to be prepared by diluting a 20% slurry. What is the amount of water required?
 (a) 500 kg (b) 1000 kg
 (c) 1500 kg (d) 2000 kg
- Q.41** The feed stream to a reactor contains ethylene 16%, oxygen 9%, nitrogen 31% and rest hydrogen chloride. If the ethylene flow is 5000 kg/h, the flow rate of oxygen is _____. (in kg/h). All percentage are by weight.
- Q.42** Carbon dioxide is added at a rate of 10 kg/h to an air stream with 0.03 percent CO₂ and the air is sampled at a sufficient distance down stream to ensure complete mixing. If the analysis shows 0.45% v/v CO₂, what is the air flow rate?
 (a) 54 kg/h (b) 1560 kg/h
 (c) 1000 kg/h (d) 560 kg/h
- Q.43** To ensure complete combustion, 20% excess air is supplied to a furnace burning natural gas. The gas composition (by volume) is methane 95%, ethane 5%. The moles of air required per mole of fuel is _____. [Rounded off to two decimal places]
- Q.44** In the manufacture of vinyl chloride (M.W = 62.5) by the pyrolysis of dichloroethane (M.W = 99), the reactor conversion is limited to 55% to reduce carbon formation, which fouls the reactor tubes. The quantity of dichloroethane fed to the reactor to produce 5000 kg/h of vinyl chloride is _____. (in kmol/h). [Rounded off to one decimal place]
- Q.45** The gas acetylene is produced according to the following reaction:
- $$\text{CaC}_2 + 2\text{H}_2\text{O} \rightarrow \text{C}_2\text{H}_2 + \text{Ca(OH)}_2$$
- The number of hours of service that can be derived from 1 kg of calcium carbide in an acetylene lamp burning 0.20 m³ gas per hour at temperature of 298 K and pressure of 100 kPa is _____. [Rounded off two decimal places]
- Q.46** A gas containing 96% ethylene and 4% butenes by volume is passed through a bed of activated carbon where 95% of the original butenes are adsorbed and none of the ethylene. In five hours of continuous operation if quantity of butenes removed is 0.6 kmol, what is the molar flow rate of the feed gas to the carbon bed?
 (a) 2.55 kmol/h (b) 3.06 kmol/h
 (c) 4.06 kmol/h (d) 3.89 kmol/h
- Q.47** A solution contains 60% ammonium nitrate, 20% urea and KCl in water by weight. What is the available nitrogen from 100 kg solution?
 (a) 23.33 kg (b) 30.33 kg
 (c) 35.33 kg (d) 45.56 kg
- Q.48** A process gas flowing at a rate of 500 m³/h at 100 kPa and 365 K contains H₂S with a partial pressure of 0.20 kPa. The gas passes to a scrubber in which 92% of the H₂S is removed. The H₂S removal rate is _____. (in kg/h)
- Q.49** A single effect evaporator is feed with 15000 kg/h of weak liquor containing 10% caustic by weight and is concentrated to get thick liquor containing 30% by weight caustic. Water evaporated in kg/h is
 (a) 5000 (b) 10000
 (c) 6250 (d) 3750
- Q.50** The ground nut seeds containing 50% oil and 30% solids are fed to expeller, the cake coming out of expeller is found to contain 70% solids and 10% oil. The percentage recovery of the oil is _____.

Common Data given for Questions (51 and 52):

An evaporator is fed with 10000 kg/h of a solution containing 15% NaCl, 10% NaOH and rest water. In the operation, water is evaporated and NaCl is precipitated as crystals. The thick liquor leaving the evaporator contains 50% NaOH, 5% NaCl and rest water.

- Q.51** kg/h water evaporated is
 (a) 6600 kg/h (b) 2000 kg/h
 (c) 1400 kg/h (d) 5000 kg/h
- Q.52** kg/h salt precipitated is
 (a) 5600 kg/h (b) 2000 kg/h
 (c) 1400 kg/h (d) 2500 kg/h

Answers		Process Calculation							
1.	(b, c)	2.	(a)	3.	(c, d)	4.	(d)	5.	(a, c, d)
8.	(2)	9.	(2)	10.	(a)	11.	(b)	12.	(b)
15.	(d)	16.	(b)	17.	(14)	18.	(c)	19.	(0.5)
22.	(a)	23.	(c)	24.	(7.13)	25.	(b)	26.	(b)
29.	(6.98)	30.	(b)	31.	(d)	32.	(687.82)	33.	(0.31)
36.	(a)	37.	(24.66)	38.	(61.34)	39.	(b)	40.	(c)
43.	(11.86)	44.	(145.5)	45.	(1.93)	46.	(b)	47.	(b)
50.	(91.43)	51.	(a)	52.	(c)	53.	(b)	54.	(558.82)
57.	(b)	58.	(b)	59.	(b)	60.	(b)	61.	(c)
64.	(c)	65.	(d)	66.	(a)	67.	(b)	68.	(b)
71.	(b)	72.	(b)	73.	(b)	74.	(94.27)	75.	(c)
78.	(b)	79.	(a)	80.	(b)	81.	(a)	82.	(d)
85.	(a)	86.	(b)	87.	(a, b, c, d)	88.	(b)	89.	(5703)
92.	(266)	93.	(2.42)	94.	(b)	95.	(b)	96.	(a)
99.	(35)	100.	(13025)	101.	(2694)	102.	(25.43)	103.	(379)
106.	(a)	107.	(58)	108.	(46)	109.	(c)	110.	(a, b, c)
113.	(26)	114.	(664.75)	115.	(a, b, c, d)	116.	(a)	117.	(c)
120.	(0)	121.	(11.7)	122.	(50)	123.	(37.2)	124.	(32.7)
127.	(68)	128.	(14)	129.	(505.6)	130.	(a)		

Explanation **Process Calculation****2. (a)**

As we increase the pressure of a gas at fixed temperature, the collision frequency increases and thus solubility goes up.

3. (c, d)

- If degree of freedom is negative then the operation is termed as overspecified.
- If the degree of freedom is positive, then the operation is termed as under specified.

6. (1)

∴ Degree of freedom (F) is given by

$$F = C - P + 2$$

where, $C = 1, P = 2$

$$\therefore F = 1 - 2 + 2 = 1$$

7. (0)

$$\begin{aligned} \therefore & F = C - P + 2 \\ \text{where, } & F = \text{Degree of freedom} \\ & C = 1 \quad (\text{Component}) \\ & P = 3 \quad (\text{Phases}) \\ \therefore & F = 1 - 3 + 2 = 0 \end{aligned}$$

8. (2)

$$\begin{aligned} \therefore & F = C - P + 2 \\ \text{where, } & C = 2, P = 2 \\ \therefore & F = 2 - 2 + 2 = 2 \end{aligned}$$

9. (2)

$$\begin{aligned} \therefore & F = C - P + 2 \\ \text{where, } & C = 2, P = 2 \\ \therefore & F = 2 - 2 + 2 = 2 \end{aligned}$$

11. (b)

$$\begin{aligned}
 M_{\text{avg}} &= \sum M_i x_i \\
 M_{\text{avg}} &= M_{\text{N}_2} \cdot x_{\text{N}_2} + M_{\text{CO}_2} \cdot x_{\text{CO}_2} \\
 31 &= 28x_{\text{N}_2} + 44x_{\text{CO}_2} \\
 x_{\text{N}_2} + x_{\text{CO}_2} &= 1 \\
 x_{\text{CO}_2} &= 1 - x_{\text{N}_2} \\
 31 &= 28x_{\text{N}_2} + 44(1 - x_{\text{N}_2}) \\
 16x_{\text{N}_2} &= 13 \\
 x_{\text{N}_2} &= 0.8125 \\
 \text{Partial pressure of N}_2 &= x_{\text{N}_2} \cdot P \\
 &= 0.8125 \times 101.325 = 82.33 \text{ kPa}
 \end{aligned}$$

M.W. of methanol = 32 g/mol,

MW of H₂O = 18 g/mol

$$\text{Mole of CH}_3\text{OH} = \frac{64}{32} = 2 \text{ moles}$$

$$\text{Mole of H}_2\text{O} = \frac{36}{18} = 2 \text{ moles}$$

$$\text{Mole fraction of methanol} = \frac{2}{4} = 0.5$$

21. (c)In 16 kg CH₄, 12 kg of carbon are present

So amount of carbon present in 64 kg of methane

$$= \frac{12}{16} \times 64 = 48 \text{ kg}$$

22. (a)

Basis: 500 ml of solution

Molecular weight of NaOH = 40

$$\text{Equivalent weight of NaOH} = \frac{40}{1} = 40$$

$$\text{Gram equivalents of NaOH} = \frac{20}{40} = 0.5 \text{ g.eq}$$

$$\text{Normality (N)} = \frac{\text{g eq. of NaOH}}{\text{Volume of solution in l}}$$

$$= \frac{0.5}{0.5} = 1$$

23. (c)

Basis: 100 kg of solution

Amount of acetic acid = 30 kg

Amount of water (solvent) = 70 kg

Molecular weight of CH₃COOH = 60

$$\text{Moles of acetic acid} = \frac{30 \times 10^3}{60} = 500 \text{ mol}$$

$$\text{Molality of solution} = \frac{\text{Moles of acetic acid}}{\text{kg of solvent}}$$

$$= \frac{500}{70} = 7.142$$

24. (7.13)

Amount of solution = 125 kg

$$\text{Moles of NaCl} = \frac{25}{58.5} = 0.427 \text{ kmol}$$

$$\text{Moles of H}_2\text{O} = \frac{100}{18} = 5.56 \text{ kmol}$$

$$\begin{aligned}
 \text{Total moles of solution} &= 0.427 + 5.56 \\
 &= 5.987 \text{ kmol}
 \end{aligned}$$

14. (b)

Isotonic solutions refers to two solution having the same osmotic pressure/or concentration across a semi-permeable membrane.

17. (14)

$$\begin{aligned}
 \text{Concentration of SO}_2 \text{ in the flue gas at NTP} \\
 &= 0.4 \text{ kg/m}^3
 \end{aligned}$$

Molecular weight,

$$\Rightarrow \text{SO}_2 = 64$$

∴ Concentration of SO₂ in ppm:

$$= \frac{0.4}{64} \times 22.4 \times 10^6 = 0.14 \times 10^6 \text{ ppm}$$

18. (c)

∴ As mass is always conserved therefore

$$aM_A = bM_B$$

$$\frac{n_b}{n_a} = \frac{M_A}{M_B}$$

Thus, M_B > M_A, then n_b < n_a where n = number of moles.

19. (0.5)

$$\therefore \text{Molality} = \frac{\text{Number of moles of solute}}{\text{Mass of solvent in kg}}$$

$$\text{Molality} = \frac{1000}{2000} = 0.5$$

20. (0.5)

Let 100 g of total mixture, i.e.

64 g → Methanol

36 g → H₂O (water)

$$\begin{aligned}\text{Mole \% NaCl in solution} &= \frac{\text{kmol NaCl}}{\text{kmol solution}} \times 100 \\ &= \frac{0.427}{5.987} \times 100 = 7.13\end{aligned}$$

25. (b)

Basis: 100 kg of ethanol-water mixture
It contains 96 kg of ethanol and 4 kg of water

$$\text{Moles of ethanol} = \frac{96}{46} = 2.087 \text{ kmol}$$

$$\text{Moles of water} = \frac{4}{18} = 0.222 \text{ kmol}$$

$$\begin{aligned}\text{Moles of azeotrope mixture} &= 2.087 + 0.222 \\ &= 2.309 \text{ kmol}\end{aligned}$$

Mole % ethanol in azeotrope mixture

$$= \frac{2.087}{2.309} \times 100 = 90.38\%$$

26. (b)

Basis: 100 cm³ of aqueous solution
Volume of ethanol in the solution = 15 cm³
Volume of water in the solution = 85 cm³
Amount of ethanol in the solution
= 15 × 0.79 = 11.85 g
Amount of water in the solution = 85 × 1 = 85 g
Weight % ethanol in the solution
= $\frac{11.85}{11.85 + 85} \times 100 = 12.23$

27. (a)

Basis: 100 kg of urea sample
Amount of N in sample = 0.45 × 100 = 45 kg
60 kg urea contains = 28 kg N
Actual urea in sample = $\frac{60}{28} \times 45 = 96.43 \text{ kg}$

28. (c)

Basis: 100 kg of sample
Amount of N in the sample = 34.5 kg
M.W. of NH₄NO₃ = 80
On the weight basis
80 kg NH₄NO₃ = 28 kg N
Amount of NH₄NO₃ in sample
= $\frac{80}{28} \times 34.5 = 98.57 \text{ kg}$

29. (6.98)

$$\text{Moles of Cl}_2 \text{ gas} = \frac{20}{71} = 0.2817 \text{ kmol}$$

Ideal gas equation

$$PV = nRT$$

$$V = \frac{nRT}{P}$$

$$= \frac{0.2817 \times 8.314 \times 298}{100}$$

$$V = 6.98 \text{ m}^3$$

30. (b)

$$\text{Moles of O}_2 = \frac{5}{32} = 0.1562 \text{ kmol}$$

$$PV = nRT$$

$$T = \frac{PV}{nR}$$

$$\text{So, } T = \frac{700 \times 1}{0.1562 \times 8.314} = 539 \text{ K}$$

31. (d)

$$PV = nRT$$

$$n = \frac{PV}{RT} = \frac{97.33 \times 2}{8.314 \times 393}$$

$$n = 0.0596 \text{ kmol}$$

$$\text{Weight of SO}_2 = 0.0596 \times 64 = 3.8144 \text{ kg}$$

32. (687.82)

A gas at 298 K in closed vessel

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

As vessel being closed

$$V_1 = V_2$$

$$\frac{P_1}{T_1} = \frac{P_2}{T_2}$$

$$\frac{131.7}{298} = \frac{303.98}{T_2}$$

$$T_2 = 687.82 \text{ K}$$

33. (0.31)

Let initial pressure = P₁

So final pressure (P₂) = 1.6P₁

Temperature and mass are constant, therefore

$$P_1 V_1 = P_2 V_2$$

$$V_2 = \frac{P_1 V_1}{P_2} = \frac{P_1 \times 0.5}{1.6 P_1} - 0.3125 \text{ m}^3$$

34. (c)

Basis: 100 kg of gas mixture

$$\text{Moles of H}_2 = \frac{11.1}{2} = 5.55 \text{ kmol}$$

$$\text{Moles of O}_2 = \frac{88.9}{32} = 2.78 \text{ kmol}$$

$$\begin{aligned}\text{Mole fraction of H}_2 &= X_{H_2} \\ &= \frac{5.55}{5.55 + 2.78} = 0.67\end{aligned}$$

$$\begin{aligned}\text{Partial pressure of H}_2 &= X_{H_2} \cdot P \\ &= 0.67 \times 100 = 67 \text{ kPa}\end{aligned}$$

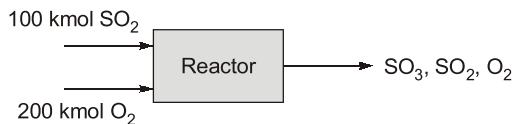
35. (b)

$$\text{Moles of CO} = \frac{M_1}{28}, \quad \text{Moles of N}_2 = \frac{M_1}{28}$$

$$\text{Total moles of the gas mixture} = \frac{2M_1}{28}$$

$$\text{Mole fraction of CO} = \frac{\frac{M_1}{28}}{\frac{2M_1}{28}} = 0.5$$

$$\begin{aligned}\text{Partial pressure of CO} &= x_{CO} \cdot P \\ &= 0.5 \times 405.3 = 202.65 \text{ kPa}\end{aligned}$$

36. (a)

For 80 kmol $\text{SO}_3 \rightarrow \text{SO}_2$ reacted is

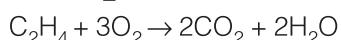
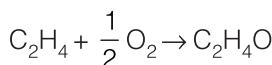
$$= 80 \times \frac{1}{1} = 80 \text{ kmol}$$

$$\begin{aligned}\% \text{ conversion of SO}_2 &= \frac{\text{kmol SO}_2 \text{ reacted}}{\text{kmol SO}_2 \text{ charged}} \times 100 \\ &= \frac{80}{100} \times 100 = 80\%\end{aligned}$$

37. (24.66)

Basis 100 mol of dry exit gases,

Reactions:



\therefore Moles of H_2O produced = moles of CO_2 produced = 5.5

$$\begin{aligned}\text{Total number of moles leaving the reactor} &= 100 + \text{moles of H}_2\text{O} \\ &= 100 + 5.5 = 105.5\end{aligned}$$

Now, analysis of exit gases on wet basis

$$\text{Ethylene} = \frac{2.3}{105.5} \times 100 = 2.18\%$$

$$\text{Ethylene oxide} = \left(\frac{0.9}{105.5} \right) \times 100 = 0.853$$

$$\begin{aligned}\therefore \% \text{ selectivity} &= \frac{\text{C}_2\text{H}_4 \text{ used for desirable reaction}}{\text{Total C}_2\text{H}_4 \text{ reacted}} \\ &= \frac{0.853}{0.853 + 0.5 \times 5.213} \times 100 = 24.66\%\end{aligned}$$

Here 5.213 is percent composition of CO_2 inert gases.

38. (61.34)

$$\begin{aligned}\% \text{ overall conversion} &= \frac{\text{Total C}_2\text{H}_4 \text{ reacted}}{\text{C}_2\text{H}_4 \text{ in feed}} \times 100 \\ &= \frac{0.853 + 0.5 \times 5.213}{0.853 + 0.5 \times 5.213 + 2.18} \times 100 = 61.34\%\end{aligned}$$

39. (b)

$$\begin{aligned}\text{Ethylene in feed} &= 0.853 + 0.5 \times 5.213 + 2.18 \\ &= 5.6395 \text{ mol}\end{aligned}$$

$$\text{Air in feed} = \frac{74.88}{0.79} = 94.785 \text{ mol}$$

\therefore Now air to ethylene mole ratio in feed is

$$= \frac{94.785}{5.6395} : 1 = 16.81 : 1$$

40. (c)

Let the unknown quantities of the 20% slurry and water be X and Y , respectively.

Material balance on Cu(OH)_2

$$X(0.2) = 2000 \times 0.05$$

$$\text{So, } X = 500 \text{ kg}$$

Balance on water

$$X(0.8) + Y = 2000 \times 0.95$$

$$Y = 1500 \text{ kg}$$

41. (2813)

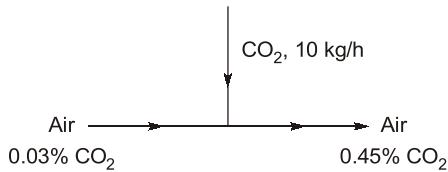
$$\% \text{ HCl} = 100 - (16 + 9 + 31) = 44$$

$$\text{Percentage ethylene} = 16 = \frac{5000}{\text{Total}} \times 100$$

$$\text{Total flow} = 5000 \times \frac{100}{16} = 31250 \text{ kg/h}$$

$$\text{So, Oxygen flow} = \frac{9}{100} \times 31250 = 2813 \text{ kg/h}$$

42. (b)



Basis: kmol/h, as percentage are by volume

$$\text{kmol/h CO}_2 \text{ introduced} = \frac{10}{44} = 0.2273$$

Let X be the air flow

Balance an CO_2 , the tie component

$$\text{CO}_2 \text{ in} = \text{CO}_2 \text{ out}$$

$$0.0003x + 0.2273 = 0.0045X$$

$$X(0.0045 - 0.0003) = 0.2273$$

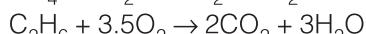
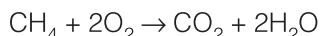
$$X = \frac{0.2273}{0.0042} = 54 \text{ kmol/h}$$

$$X = 54 \times 29 = 1560 \text{ kg/h}$$

43. (11.86)

Basis: 100 mol gas, as the analysis is volume percentage.

Reaction:



Stoichiometric moles of O_2 required

$$= 95 \times 2 + 5 \times 3.5 = 207.5$$

With 20% excess, moles of O_2 required

$$= 1.2 \times 207.5 = 249$$

$$\text{Moles of air} = \frac{249}{0.21} = 1185.7$$

$$\text{As per mole of fuel} = \frac{1185.7}{100} = 11.86 \text{ mol}$$

44. (145.5)



$$\text{kmol/h vinyl chloride produced} = \frac{5000}{62.5} = 80$$

From stoichiometric equation, 1 kmol DCE produces 1 kmol VC. Let X be DCE feed in kmol/h

$$\text{Percent conversion} = \frac{80}{X} \times 100 = 55$$

$$X = \frac{80}{0.55} = 145.5 \text{ kmol/h}$$

45. (1.93)

$$\text{Moles of CaC}_2 = \frac{1}{64} = 0.01562 \text{ kmol}$$

From reaction

$$1 \text{ kmol CaC}_2 = 1 \text{ kmol C}_2\text{H}_2$$

$$\text{Moles of C}_2\text{H}_2 \text{ produced} = 0.01562 \text{ kmol}$$

$$PV = nRT$$

Volume of C_2H_2 gas produced

$$= \frac{0.01562 \times 8.314 \times 298}{100} = 0.386 \text{ m}^3$$

Number of hours of service

$$= \frac{\text{Volume of acetylene gas}}{\text{Burning rate of acetylene}}$$

$$= \frac{0.386}{0.20} = 1.935 \text{ h}$$

46. (b)

$$\text{Butenes removed} = \frac{0.6}{5} = 0.12 \text{ kmol/h}$$

Let y be the molar flow rate of gas to the carbon bed

Butenes in the gas fed = $0.04y$ kmol/h

$$\begin{aligned} \text{Butenes adsorbed} &= 0.98 \times 0.04y \\ &= 0.0392y \text{ kmol/h} \end{aligned}$$

$$0.0392y = 0.12$$

$$y = \frac{0.12}{0.0392} = 3.06 \text{ kmol/h}$$

Molar flow rate of the gas to carbon bed

$$= 3.06 \text{ kmol/h}$$

47. (b)

Basis: 100 kg of solution

It contains 60 kg ammonium nitrate and 20 kg urea.

$$1 \text{ kmol NH}_4\text{NO}_3 = 2 \text{ kmol N}$$

$$80 \text{ kg NH}_4\text{NO}_3 = 28 \text{ kg N}$$

$$\begin{aligned} \text{Nitrogen available from NH}_4\text{NO}_3 &= \frac{28}{80} \times 60 \\ &= 21 \text{ kg} \end{aligned}$$

$$1 \text{ kmol NH}_4\text{CONH}_2 = 2 \text{ kmol N}$$

$$60 \text{ kg NH}_4\text{CONH}_2 = 28 \text{ kg N}$$

$$\text{Nitrogen available from area} = \frac{28}{60} \times 20 = 9.33 \text{ kg}$$

Total nitrogen available from solution

$$= 21 + 9.33 = 30.33 \text{ kg}$$

48. (1.03)

Partial pressure of $\text{H}_2\text{S} = 0.20 \text{ kPa}$

$$\text{Pressure fraction of } \text{H}_2\text{S} = \frac{0.20}{100} = 0.2 \times 10^{-2}$$

For ideal gas

Pressure fraction = Mole fraction = 2×10^{-3}

Molar flow rate of process gas

$$= \frac{500 \times 100}{8.314 \times 365} = 16.47 \text{ kmol/h}$$

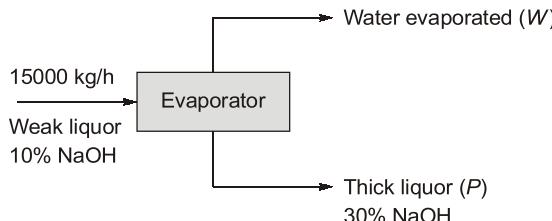
H_2S in the process gas = $2 \times 10^{-3} \times 16.47$

$$= 0.033 \text{ kmol/h}$$

H_2S removed in the scrubber = 0.92×0.033

$$= 0.03 \text{ kmol/h}$$

H_2S removal rate = $0.03 \times 34 = 1.03 \text{ kg/h}$

49. (b)

Overall material balance

$$15000 = W + P \quad \dots(i)$$

Material balance of NaOH

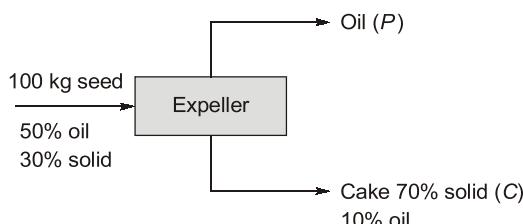
$$15000 \times 0.1 = P \times 0.30$$

$$P = \frac{1500}{0.30} = 5000 \text{ kg/h}$$

From equation (i)

$$15000 = W + 5000$$

$$W = 10000 \text{ kg/h}$$

50. (91.43)

Overall material balance

$$100 = P + C$$

Material balance of solid

$$0.30 \times 100 = 0.70 \times C$$

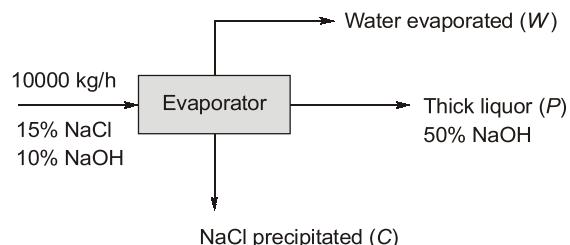
$$C = 42.85 \text{ kg}$$

Material balance of oil

$$0.50 \times 100 = 0.10 \times C + P$$

(Oil recovered) $P = 45.71 \text{ kg}$

$$\begin{aligned} \% \text{ recovery of the oil} &= \frac{\text{kg oil recovered}}{\text{kg oil in seeds}} \times 100 \\ &= \frac{45.71}{50} \times 100 = 91.43\% \end{aligned}$$

51. (a)

Overall material balance

$$10000 = W + P + C$$

Material balance of NaOH

$$0.10 \times 10000 = P \times 0.50$$

$$P = 2000 \text{ kg/h}$$

Material balance of NaCl

$$0.15 \times 10000 = 0.05 \times 2000 + C$$

$$C = 1400 \text{ kg/h}$$

We have,

$$P + W + C = 10000$$

$$1400 + 2000 + W = 10000$$

$$W = 6600 \text{ kg/h}$$

52. (c)

NaCl precipitated

$$0.15 \times 10000 = 0.05 \times P + C$$

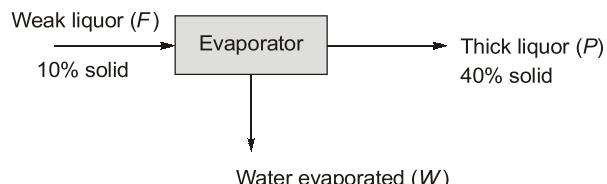
where, $P = 2000 \text{ kg/h}$

$$C = 1500 - 100 = 1400 \text{ kg/h}$$

53. (b)

Case I:

Basis: 100 kg/h of solid handling capacity of the evaporator



Material balance of solids

$$0.1 \times F = P \times 0.4$$

Given, $0.1 \times F = 100$

$$\text{So, } P = \frac{100}{0.4} = 250 \text{ kg/h}$$